

## Well test analysis of horizontal wells in a two-layered reservoir system: Mathematical derivation

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### *Abstract*

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*In this paper, a well test analysis procedure is discussed for a two-layered oil reservoir drained from each layer by a horizontal well. Reservoir mathematical model are derived for each layer so that analysis can be done strictly for each layered reservoir. Procedures for obtaining all the directional permeabilities, wellbore skin, degree of crossflow and individual layers average pressures are discussed for a pressure drawdown test procedure*

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### Nomenclature

$$p_D = \frac{kh\Delta p}{141.2q\mu B}; t_D = \frac{0.001056 kt}{\mu\phi c_t L^2}; i_D = \frac{2i}{L} \sqrt{\frac{k}{k_i}},$$

$i$  = positions along  $x$  or  $y$  or  $z$  axes,  $ft$ ;

$$h_D = 1/L_D;$$

$\Delta$  = drop;

$p$  = pressure,  $psi$ ;

$k$  = permeability,  $md$ ;

$h$  = pay thickness,  $ft$ ;

$t$  = time, hours;

$q$  = flow rate, STB/Day;

$\mu$  = oil viscosity,  $cp$ ;

$B$  = oil formation volume factor, bbl/STB;

$c_t$  = total fluid compressibility,  $1/psi$ ;

$L$  = well length,  $ft$ ;

$erf$  = error function;

$\tau$  = dimensionless dummy time variable  $t_D p'_D$  dimensionless pressure derivative.

### Subscripts

$x, y, z = x, y, \text{ or } z, \text{ directions}; D = \text{dimensionless}; w = \text{wellbore}; e = \text{external}$

## 1.0 Introduction

Horizontal well test and analysis procedures have been adequately reported in the literature especially in the late 1990's [1, 2, 3,4]. At first, test analyses procedures were modeled in the form of the conventional test analyses procedures such as the (Horner's) buildup and pressure drawdown plots. Later, dimensionless pressure derivative plots were introduced [5, 8], to solve test analyses shortcomings associated with the conventional test analyses methods.

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The major aims of all transient test analyses are to evaluate wellbore condition, reservoir heterogeneity and reservoir boundary types. This information helps in planning well work over or repair, well location strategy for optimum recovery, production or injection profiling and determination of source of available reservoir energy (boundary types).

Layered reservoirs present peculiar problems. Apart from possessing more than one permeability distribution, the nature of their interfaces have to be established to determine a more technically suitable completion pattern for both economic benefits and high productivity. The interface may be permeable or not permeable. Permeable interfaces allow crossflow while no crossflow occurs if the interfaces are not permeable. Well completion strategies in layered reservoirs with crossflow and no crossflow interfaces have been discussed for vertical wells [9, 10]. Not so much similar efforts have been made for horizontal wells, but many authors have discussed analytical methods of delineating flow boundaries [1, 2, 3, 8, 11, 12, 13]. These methods can be used to determine both lateral and vertical extents of the reservoir from a horizontal well test. The remaining aspect yet to be discussed in as much detail remains the degree of crossflow determination. The degree of crossflow determines whether to crossflow the individual layers or commingle all the layers.

In this paper, a two-layered oil reservoir drained collectively and individually, with a horizontal well will be modeled mathematically and a detailed test analysis procedure based on the model will be discussed. Major information that will be derived from the well test analysis are (1) directional permeabilities,  $k_x$ ,  $k_y$ , and  $k_z$ , (2) wellbore damage skin factor,  $s$ , (3) average reservoir pressure,  $p_e$ , (4) minimum wellbore pressure,  $p_{wm}$ , for oil production from only one layer, and (5) degree of crossflow,  $\beta$ . Both layer dimensionless pressure distribution and their derivatives will be derived and utilized.

## 2.0 Reservoir and Mathematical model descriptions

An anisotropic two-layered reservoir system is assumed. As shown below in Figure 2.1, each layer is penetrated with a horizontal well.

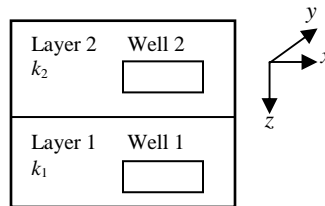


Figure 2.1: Layered Reservoir Model

For a permeable interface let the propensity of interface fluid crossflow be given by the index  $\beta$ , where  $\xi \leq \beta \leq \infty$ , practically, and  $\xi$  is a small positive value, greater than zero. As will be clear later, for an isotropic reservoir layers if  $\beta = 1$ , then the interface will experience no crossflow even though it may be permeable except created artificially under large pressure drop. Lower values of  $\beta$  mean that the interface will experience limited crossflow, while larger values mean that the interface will experience sufficient crossflow. [14] describes the mathematical development of the pressure distribution for the reservoir system shown in Figure 2.1 above. The layers dimensionless pressure distribution expressions according to the references are as follows for laterally infinite layers:

**(1) Upper Layer (Layer 2)**

$$p_{D2} = \frac{E_2 \sqrt{\pi \beta}}{2} \sqrt{\frac{k}{k_y}} \int_0^{t_D} \left[ \operatorname{erf} \frac{\sqrt{k/k_x} + x_D}{2\sqrt{\beta \tau}} + \operatorname{erf} \frac{\sqrt{k/k_x} - x_D}{2\sqrt{\beta \tau}} \right] \frac{e^{-(y_D - y_{wD})^2 / 4\beta \tau}}{\sqrt{\tau}} \quad (2.1)$$

$$\times \sum_{n=1}^{\infty} \exp\left(-\frac{(2n-1)^2 \pi^2 \tau}{4h_D^2} \sin \frac{(2n-1)\pi z_D}{2h_D} \sin \frac{(2n-1)\pi z_{wD}}{2h_D}\right) d\tau$$

where  $\beta = (\phi_1 c_{11} \mu_1 L_1^2 k_2) / ((\phi_2 c_{12} \mu_2 L_2^2 k_1))$  (2.2)

**(2) Lower Layer (Layer 1)**

$$p_{D1} = \frac{E_1 \sqrt{\pi}}{2} \sqrt{\frac{k}{k_y}} \int_0^{t_D} \left[ \operatorname{erf} \frac{\sqrt{k/k_x} + x_D}{2\sqrt{\tau}} + \operatorname{erf} \frac{\sqrt{k/k_x} - x_D}{2\sqrt{\tau}} \right] \frac{e^{-(y_D - y_{wD})^2 / 4\tau}}{\sqrt{\tau}} \quad (2.3)$$

$$\times \sum_{n=1}^{\infty} \exp\left(-\frac{(2n+1)^2 \pi^2 \tau}{4h_D^2} \cos \frac{(2n+1)\pi z_D}{h_D} \cos \frac{(2n+1)\pi z_{wD}}{h_D}\right) d\tau$$

In both Equations 2.1 and 2.3, the effects of the individual layers boundaries along the  $-x$  and  $-y$  axes have not been felt and are considered infinite. Only the interface effects (along the top or bottom  $-z$  axis of the layers) are assumed now felt. When all the boundaries are felt, the following equations are then used in place of Equations 2.1 and 2.3, for central well location along the  $x$ -axis, according to [15]:

$$p_{D2} = \frac{4\pi E_2 \beta}{y_{eD} x_{eD}} \int_0^{t_D} \left[ 1 + \frac{2x_{eD}}{\pi} \sum_{n=1}^{\infty} \frac{1}{n} \exp\left(-\frac{n^2 \pi^2 \tau \beta}{x_{eD}^2}\right) \sin \frac{n\pi}{x_{eD}} \cos \frac{n\pi x_{wD}}{x_{eD}} \cos \frac{n\pi x_D}{x_{eD}} \right] \quad (2.4)$$

$$\times \left[ 1 + 2 \sum_{m=1}^{\infty} \exp\left(-\frac{m^2 \pi^2 \tau \beta}{y_{eD}^2}\right) \cos \frac{m\pi y_{wD}}{y_{eD}} \cos \frac{m\pi y_D}{y_{eD}} \right]$$

$$\times \sum_{l=1}^{\infty} \exp\left(-\frac{(2l-1)^2 \pi^2 \tau \beta}{4h_D^2}\right) \sin \frac{(2l-1)\pi z_{wD}}{2h_D} \sin \frac{(2l-1)\pi z_D}{2h_D} d\tau$$

$$p_{D1} = \frac{4\pi E_1}{y_{eD} x_{eD}} \int_0^{t_D} \left[ 1 + \frac{2x_{eD}}{\pi} \sum_{n=1}^{\infty} \frac{1}{n} \exp\left(-\frac{n^2 \pi^2 \tau}{x_{eD}^2}\right) \sin \frac{n\pi}{x_{eD}} \cos \frac{n\pi x_{wD}}{x_{eD}} \cos \frac{n\pi x_D}{x_{eD}} \right] \quad (2.5)$$

$$\times \left[ 1 + 2 \sum_{m=1}^{\infty} \exp\left(-\frac{m^2 \pi^2 \tau}{y_{eD}^2}\right) \cos \frac{m\pi y_{wD}}{y_{eD}} \cos \frac{m\pi y_D}{y_{eD}} \right]$$

$$\times \sum_{l=1}^{\infty} \exp\left(-\frac{(2l+1)^2 \pi^2 \tau}{4h_D^2}\right) \cos \frac{(2l+1)\pi z_{wD}}{2h_D} \cos \frac{(2l+1)\pi z_D}{2h_D} d\tau$$

In other words, Equations 2.4 and 2.5 prevail long after the prevalence of 2.1 and 2.3 if (1) the interface experiences no crossflow or limited crossflow, (2) large layers  $k_h/k_v$  ratios and (3) low layers wells withdrawal or injection rates. Otherwise, production of fluid from or injection into one of the two layers would produce the effects of one enlarged reservoir in which case all the parameters would now be the average or equivalent sum of the parameters of all the layers. Furthermore, the flow across the interface would now be dependent upon the degree of communication,  $\beta$ , between the layers. By equating dimensionless pressures and flow velocities at the interface, the expression for E can be derived as follows if Equations 2.1 and 2.3 are used [14, 15]:

$$E = \frac{2}{\sqrt{\pi}} \left[ \begin{array}{c} \int_{z_{wD1}}^{h_{D1}} I_{11} dz_D + \int_{h_{D1}}^{h_D} I_{22} dz_D \\ \int_{z_{wD1}}^{h_{D1}} I_{11}^2 dz_D + \int_{h_{D1}}^{h_D} I_{22}^2 dz_D \end{array} \right] \quad (2.6)$$

where

$$I_{11} = \sqrt{\frac{k}{k_y}} \int_0^{t_D} \left[ \operatorname{erf} \frac{\sqrt{k/k_x} + x_D}{2\sqrt{\tau}} + \operatorname{erf} \frac{\sqrt{k/k_x} - x_D}{2\sqrt{\tau}} \right] \frac{e^{-(y_D - y_{wD})^2 / 4\tau}}{\sqrt{\tau}} \quad (2.7)$$

$$\times \sum_{n=1}^{\infty} \exp\left(-\frac{(2n+1)^2 \pi^2 \tau}{4h_D^2}\right) \cos \frac{(2n+1)\pi(z_D = h_{D1})}{h_D} \cos \frac{(2n+1)\pi z_{wD}}{h_D} d\tau$$

and

$$I_{22} = \sqrt{\beta} \sqrt{\frac{k}{k_y}} \int_0^{t_D} \left[ \operatorname{erf} \frac{\sqrt{k/k_x} + x_D}{2\sqrt{\beta\tau}} + \operatorname{erf} \frac{\sqrt{k/k_x} - x_D}{2\sqrt{\beta\tau}} \right] \frac{e^{-(y_D - y_{wD})^2 / 4\beta\tau}}{\sqrt{\tau}} \quad (2.8)$$

$$\times \sum_{n=1}^{\infty} \frac{(2n-1)\pi}{2} \exp\left(-\frac{(2n-1)^2 \pi^2 \beta\tau}{4h_D^2}\right) \cos \frac{(2n-1)\pi(z_D = h_{D1})}{2h_D} \sin \frac{(2n-1)\pi z_{wD}}{2h_D} d\tau$$

### 2.1 Well test analysis Mathematical model

For application in well test analysis, assuming Well 1, the solution to Equation 2.3 is written as

$$p_{D1} = -\frac{h_D}{4} \sqrt{\frac{kk}{k_y k_z}} \operatorname{Ei}\left(-\frac{r_D^2}{4t_D}\right) + \frac{E\sqrt{\pi}}{2} \sqrt{\frac{k}{k_y}} \int_0^{t_D} \left[ \operatorname{erf} \frac{\sqrt{k/k_x} + x_D}{2\sqrt{\tau}} + \operatorname{erf} \frac{\sqrt{k/k_x} - x_D}{2\sqrt{\tau}} \right] \frac{e^{-(y_D - y_{wD})^2 / 4\tau}}{\sqrt{\tau}} \quad (2.9)$$

$$\times \sum_{n=1}^{\infty} \exp\left(-\frac{(2n+1)^2 \pi^2 \tau}{4h_D^2}\right) \cos \frac{(2n+1)\pi z_D}{h_D} \cos \frac{(2n+1)\pi z_{wD}}{h_D} d\tau.$$

Equation 2.9 is obtained by superposing the infinite-acting (radial) flow period and the early linear flow period. During the infinite-acting flow,  $E = 0$  since no external physical boundary has been encountered. According to [5, 6, 7] the pressure derivative for Equation 2.9 is

$$t_D p_D' = -\frac{h_D}{4} \sqrt{\frac{kk}{k_y k_z}} e^{-r_D^2 / 4t_D} + E \frac{\sqrt{\pi} h_D}{2} \sqrt{\frac{k}{k_y}} \left[ \operatorname{erf} \frac{\sqrt{k/k_x} + x_D}{2\sqrt{\tau}} + \operatorname{erf} \frac{\sqrt{k/k_x} - x_D}{2\sqrt{\tau}} \right] e^{-(y_D - y_{wD})^2 / 4\tau} \quad (2.10)$$

$$\times \sum_{n=1}^{\infty} \exp\left(-\frac{(2n+1)^2 \pi^2 \tau}{4h_D^2}\right) \cos \frac{(2n+1)\pi z_D}{h_D} \cos \frac{(2n+1)\pi z_{wD}}{h_D}$$

Note that Equations 2.1, 2.3, 2.4, 2.5, 2.9 and 2.10 do not depend on the ratio  $\sqrt{k/k_y}$  as a result of multiplication by  $E$ .

## 2.2 Well test analysis procedure

For various of  $h_D$ ,  $r_D$ ,  $\sqrt{k/k_x}$ ,  $y_D$  and  $y_{wD}$  ( $= r_{wD}$ ), type curves can be produced for  $p_{D1}$  versus  $t_D$  and  $t_D p_{D1}$  versus  $t_D$ , respectively, on log-log axes. A plot of  $t_D p_{D1}$  against  $e^{-r_D^2/4t_D}$  and a plot of  $p_D$  against  $Ei(-r_D^2/4t_D)$  on linear axes yield the same slope of  $(-0.25h_D\sqrt{kk/k_y k_z})$ . However, in a well test only pressures,  $p$ , and flow times,  $t$ , are read directly; other parameters to be obtained from the well test are calculated. If the values of  $h_D$  and  $\sqrt{k/k_x}$  are obtained from type-curve matching, then with the slope obtained from the plots above there are now three equations and three unknowns to be solved for. These unknowns are  $k_x$ ,  $k_y$ , and  $k_z$  and the three equations are

$$h_D = \frac{2h}{L} \sqrt{\frac{k}{k_z}} \quad (2.11)$$

$$(-0.25h_D\sqrt{kk/k_y k_z} = A) \quad (2.12)$$

and

$$\sqrt{k/k_x} = B \quad (2.13)$$

Solving the three equations simultaneously, we have

$$k_x = \frac{8A^{3/2}}{h_D^{3/2} B^{3/2}}, \quad k_y = \frac{8A^{1/2}}{h_D^{5/2} B^{1/2} L^2}, \quad \text{and} \quad k_z = \frac{8A^{3/2}}{h_D^{1/2} B^{-5/2} L^2}, \quad (2.14)$$

## 2.3 Behaviour of $E$

At early dimensionless times,  $p_D$  is not affected by  $E$ , since no boundary is felt yet. For all well parameters, values of  $E$  remain constant beyond the early flow period [14, 16]. Negligible values of  $E$  are obtained for large values of  $h_D$ , showing that the factor  $E$  becomes negligible as the layers thickness becomes larger. In other words, the layers  $p_D$  values still behave as if the pay thickness are infinite. Note that for reservoirs without crossflow,  $E = 1$  for all expressions to be valid. During the period beyond radial flow, i.e., when  $E$  is constant, it therefore means that

$$E = \text{constant} \quad (2.15)$$

Hence

$$E - \text{constant} = 0 \quad (2.16)$$

where  $\text{constant}$  is the constant value obtained beyond the early radial flow period. Equation 2.15 is valid only at  $t_D \geq t_{De}$  and  $t_{De}$  is the least value of  $t_D$  that satisfies Equation 2.15. It may also be the dimensionless time when the interface is felt. Thus, for any set of wellbore and reservoir layers parameters a particular value of  $\beta$  that satisfies Equation 2.16 can be estimated numerically using the Newton-Raphson scheme as follows: Assume that  $\beta = 0$ , the worst scenario. Obtain

$$E' = \frac{\partial E}{\partial \beta} \quad (2.17)$$

Then

$$\beta_{i+1} = \beta_i - \frac{E(\beta = 0)}{E'(\beta = 0)} \quad (2.18)$$

If  $|\beta_{i+1} - \beta_i| \approx \text{epsilon}$ , then  $\beta_i$  is the degree of crossflow across the interface.

## 3.0 Individual reservoir layers average pressure

The general relationship for the flowing well pressure and reservoir layers pressure is given as

$$p(x, y, z, t) = p_e - \frac{141.2q\mu B}{kh} (p_D + s) \quad (3.1)$$

where  $s$  is the wellbore skin and  $p_D$  is given by Equation 3.1, assuming Well 1 is the monitoring well. From Equation 3.1, it is expected that the growth of  $p_D$ , occasioned by the exponential integral is interrupted the moment the interface is felt and beyond. If the dimensionless time at which the constant value is attained is  $t_{Dss}$ , then

$$p_{D1} = -\frac{h_D}{4} \sqrt{\frac{kk}{k_y k_z}} Ei\left(-\frac{r_D^2}{4t_D}\right) + \frac{E\sqrt{\pi}}{2} \sqrt{\frac{k}{k_y}} \int_{t_{De}}^{t_{Dss}} \left[ \operatorname{erf} \sqrt{\frac{k/k_x + x_D}{2\sqrt{\tau}}} + \operatorname{erf} \sqrt{\frac{k/k_x - x_D}{2\sqrt{\tau}}} \right] \frac{e^{-(y_D - y_{wD})^2/4\tau}}{\sqrt{\tau}} d\tau \quad (3.2)$$

$$\times \sum_{n=1}^{\infty} \exp\left(-\frac{(2n+1)^2 \pi^2 \tau}{4h_D^2} \cos \frac{(2n+1)\pi z_D}{h_D} \cos \frac{(2n+1)\pi z_{wD}}{h_D}\right) d\tau$$

At  $t_D > t_{Dss}$  flow is now propagated beyond the interface in the  $x$ - $y$  plane for highly compressible oil. The rapidity at which this is attained depends on the degree of crossflow of the interface. Note that in Equation 3.2,  $p_{D1}$  does not depend on dimensionless time.

Using Equation 3.2 in Equation 3.1 and for a constant drawdown or injection rate, a plot of  $p(x, y, z, t)$  recorded at the surface against  $p_D$  yields a straight line with intercept  $p_e$  on the vertical axis. The intercept should be obtained by extrapolating the portion of the curve that is parallel to the  $p_D$  axis; that is, the minimum wellbore pressure,  $p_{wm}$ , required for fluid production or injection from the bottom layer only and at the prevailing rate. The slope of the curve,  $m = 141.2q\mu B/kL$ , can be used to calculate  $k$ ,  $kL$ ,  $k/\mu$ , etc.

### 3.1 Estimation of Skin Factor, $s$

To permit estimation of the skin factor,  $s$ , Equation 3.2 is written to include the skin factor and oil field units as follows:

$$p = p_e - \frac{1626q\mu B}{kL} \left\{ \frac{h_D}{4} \sqrt{\frac{kk}{k_y k_z}} \left( \log + \log \frac{k}{\phi\mu_i L^2} - 2.625 \right) + \frac{E\sqrt{\pi}}{2} \sqrt{\frac{k}{k_y}} \int_{t_{Dint}}^{t_{Dhr}} \left[ \operatorname{erf} \sqrt{\frac{k/k_x + x_D}{2\sqrt{\tau}}} + \operatorname{erf} \sqrt{\frac{k/k_x - x_D}{2\sqrt{\tau}}} \right] \frac{e^{-(y_D - y_{wD})^2/4\tau}}{\sqrt{\tau}} d\tau + 0.87s \right. \left. \sum_{n=1}^{\infty} \exp\left(-\frac{(2n+1)^2 \pi^2 \tau}{4h_D^2} \cos \frac{(2n+1)\pi z_D}{h_D} \cos \frac{(2n+1)\pi z_{wD}}{h_D}\right) d\tau + 0.87s \right\} \quad (3.3)$$

After flowing the well for 1hr, Equation 3.3 is now given as:

$$p_{1hr} = p_e - \frac{1626q\mu B}{kL} \left\{ \frac{h_D}{4} \sqrt{\frac{kk}{k_y k_z}} \left( \log \frac{k}{\phi\mu_i L^2} - 2.625 \right) + \frac{E\sqrt{\pi}}{2} \sqrt{\frac{k}{k_y}} \int_{t_{Dint}}^{t_{D1hr}} \left[ \operatorname{erf} \sqrt{\frac{k/k_x + x_D}{2\sqrt{\tau}}} + \operatorname{erf} \sqrt{\frac{k/k_x - x_D}{2\sqrt{\tau}}} \right] \frac{e^{-(y_D - y_{wD})^2/4\tau}}{\sqrt{\tau}} d\tau + 0.87s \right. \left. \sum_{n=1}^{\infty} \exp\left(-\frac{(2n+1)^2 \pi^2 \tau}{4h_D^2} \cos \frac{(2n+1)\pi z_D}{h_D} \cos \frac{(2n+1)\pi z_{wD}}{h_D}\right) d\tau + 0.87s \right\} \quad (3.4)$$

Solving,

$$s = 1.15 \left\{ \frac{(p_e - p_{1hr})}{m} \left[ \frac{h_D}{4} \sqrt{\frac{kk}{k_y k_z}} \left( \log \frac{k}{\phi\mu_i L^2} - 2.625 \right) + \frac{E\sqrt{\pi}}{2} \sqrt{\frac{k}{k_y}} \int_{t_{Dint}}^{t_{D1hr}} \left[ \operatorname{erf} \sqrt{\frac{k/k_x + x_D}{2\sqrt{\tau}}} + \operatorname{erf} \sqrt{\frac{k/k_x - x_D}{2\sqrt{\tau}}} \right] \frac{e^{-(y_D - y_{wD})^2/4\tau}}{\sqrt{\tau}} d\tau + 0.87s \right. \left. \sum_{n=1}^{\infty} \exp\left(-\frac{(2n+1)^2 \pi^2 \tau}{4h_D^2} \cos \frac{(2n+1)\pi z_D}{h_D} \cos \frac{(2n+1)\pi z_{wD}}{h_D}\right) d\tau + 0.87s \right] \right\} \quad (3.5)$$

where  $m = 162.6q\mu B/kL$ . Note that in Equation 3.5,  $s$  does not depend on dimensionless time since it is evaluated within constant dimensionless time interval  $t_{De}$  and  $t_{D1hr}$ . The  $p_{1hr}$  must be obtained from the straight line on a plot of  $p_{wf}$  against  $\log t$ .

All infinite summations are performed at the wellbore, i.e., at  $n = 1$ . The integrals can be evaluated numerically.

#### 4.0 Conclusion

Horizontal well analysis has been discussed for a layered reservoir with crossflow interface. For a pressure draw down test analysis procedure, the following conclusions can be deduced:

1. Type curve matching is required to obtain  $h_D$  and  $\sqrt{k/k_x}$ . Even though the degree of crossflow,  $\beta$ , can be obtained from type curve matching, it can also be obtained from Newton-Raphson scheme.
2. A plot of subsurface pressures versus computed dimensionless pressures is made to read the layers average pressures. This is against conventional approaches for obtaining average reservoir pressures in the literature.
3. The plot above can also be used to estimate the minimum bottomhole pressure to guarantee oil production from only one layer under a specific rate regime.
4. All directional permeabilities are inversely proportional to dimensionless thickness in varying degrees.
5. The slopes of dimensionless pressure against  $Ei(-r_D^2/4t_D)$  and dimensionless pressure derivative against  $\exp(-r_D^2/4t_D)$  are the same.

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