

## Pressure Distribution in a Layered Reservoir with Lateral Wells

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### Abstract.

The production of oil and gas from a layered reservoir using lateral wells at economic rates has been a major problem to both the reservoir and production engineers. The problem manifests in such wells when they cannot deliver fluid at the desired rates and volumes, good enough to justify the level of investment (measured by discovery, drilling and completion efforts.) This is often traceable to lack of good understanding of fluid dynamics in layered reservoirs when they are drilled with lateral drainholes. In this paper, mathematical models are constructed to study pressure distribution in a layered reservoir, with and without crossflow, containing lateral wells. The pressure distributions are utilized to investigate the wellbore, reservoir layers and layers fluid conditions best suited for optimum oil recovery.

pp 135 - 146

### 1.0 Introduction

When a reservoir is layered then the reservoir has more than one clearly identifiable permeability distribution and an interface. If the layers are in communication (cross flow), fluid will flow into the layer of larger permeability, and therefore, the layer fluids can be produced through one well. On the other hand, if the layers are not in communication (no cross flow) then the layers fluids are either commingled or produced separately.

In this paper, the candidacy of lateral wells, as oil producers or fluid injectors in a layered reservoir, is investigated in terms of well bore pressure distribution.

Pressure distribution studies in layered reservoirs, for now, are more popular than vertical wells [1], [2]. But [3] and [4] proposed theoretical studies of fluid flow in multi-layered reservoirs involving horizontal wells basically to permit identification of flow periods, reservoir layers boundaries and well bore conditions. These authors modelled only one horizontal well in a stratified reservoir as a case of extended single layer reservoir with crossflow. Recently [5] and [6] utilized pressure distribution in a layered reservoir to study the effect of length on wellbore productivities. Test analysis of pressure from layered reservoirs was discussed by [6]. We intend, in this paper, to extend the frontiers of [5] and [6]. Green's and source functions developed in [7] and [9] will be utilized to derive all pressure distribution expressions.

### 2.0 Layered Reservoir and Mathematical Models Descriptions

The stratified model shown in Figure 1 consists of two drainholes. There are two clearly identifiable layers. Between the identified layers, there is an interface, which may be permeable or impermeable. Each layer contains fluid of small and constant compressibility but the layers do not necessarily have the same viscosity. The wells are assumed to be parallel to a pair of top and bottom no-flow boundaries and each is located in a semi-infinite rectangular drainage region. The wells produce or receive fluid at a constant rate across the sand face of each wellbore. Each layer's pressure before production, injection or buildup is  $p_i$ . We wish to derive a relationship between  $p_i$ , reservoir layers, layers' fluids, and wellbore properties with time, to gain an insight into the fluid dynamics in the layered reservoir subject to a pressure transient. The wells have radii  $r_{wj}$  along the  $y$  and  $z$  axes, and lengths  $L_j$  along the  $x$ -axis. The widths of the wells (along the  $y$ -axis) are  $y_{wj} = 0$  to  $y_{wj} = \infty$  in width; that is, each layer is semi-infinite in dimension. Each well is  $z_{wj}$  away from its no-flow vertical boundary and each layer is  $h_{wj}$  thick. Therefore, the top of the bottom layer is the location of the interface. The reservoir layers are considered to be largely anisotropic, and all permeabilities are considered to be independent of pressure. However, production or injection pressures are assumed to be above



bubble point of oil. As there are no external recharging boundaries either at the top or bottom of reservoir, the energy for fluid flow is derived strictly from the dissolved gas in the oil or from fluid injection pressure. Skin effects and wellbore storage problems are considered negligible.

The wells therefore, experience source strengths, along the x-axis, from an infinite slab in an infinite reservoir along y-axis. The z-axis sources are, however, dependent on whether the interface is permeable (crossflow) or not (no crossflow.) For no crossflow, the source strengths from the z-axis are originating from infinite plane sources in infinite slab reservoirs.

For crossflow layers, the z-axis represents a mixed boundary situation as shown in Figure 2. Here the interface is assumed to be similar to a partially-constant-pressure boundary. Therefore, if the individual layers are considered separately, the top layer has a partially recharging boundary at the top, similar to a gas cap. Therefore, the z-axis source functions for each layer must contain a weighting factor which accounts for his dual-natured boundary effects at the interface. Considering the above description, the following source functions can be written as discussed in [7], [9] and [16].

x-axis

$$s(x_{Dj}, t_{Dj}) = \frac{1}{4} \left[ \operatorname{erf} \left( \frac{1+x_{Dj}}{2\sqrt{t_{Dj}}} \right) \right] + \operatorname{erf} \left( \frac{1-x_{Dj}}{2\sqrt{t_{Dj}}} \right) \tag{2.1}$$

y-axis

$$s(y_{Dj}, t_{Dj}) = \frac{1}{2\sqrt{\pi t_{Dj}}} e^{-\frac{(y_{Dj}-y_{wDj})^2}{4t_{Dj}}} \tag{2.2}$$

z-axis

(i) Crossflow

$$s(z_{Di}, t_{Di}) = \frac{E_i}{h_{Di}} \sum_{n=1}^{\infty} \exp \left( -\frac{(2n+1)^2 \pi^2 t_{Di}}{4h_{Di}^2} \right) \frac{\cos \frac{(2n+1)\pi z_{Di}}{h_{Di}} \cos \frac{(2n+1)\pi z_{wDi}}{h_{Di}}}{h_{Di}} \tag{2.3a}$$

$$s(z_{Di+1}, t_{Di+1}) = \frac{E_{i+1}}{h_{Di+1}} \sum_{n=1}^{\infty} \exp \left( -\frac{(2n-1)^2 \pi^2 t_{Di+1}}{4h_{Di+1}^2} \right) \frac{\sin \frac{(2n-1)\pi z_{Di+1}}{2h_{Di+1}} \sin \frac{(2n-1)\pi z_{wDi+1}}{2h_{Di+1}}}{2h_{Di+1}} \tag{2.3b}$$

where  $E_j$  is the desired weighting factor.  $j = \text{layer } i \text{ or } i + 1$ .

(ii) No Crossflow

$$s(z_{Dj}, t_{Dj}) = \frac{1}{h_{Dj}} \left[ 1 + 2 \sum_{n=1}^{\infty} \exp \left( -\frac{n^2 \pi^2 t_{Dj}}{4h_{Dj}^2} \right) \cos \frac{n\pi z_{Dj}}{h_{Dj}} \cos \frac{n\pi z_{wDj}}{h_{Dj}} \right] \tag{2.4}$$

It should be noted, however, that for the z-axis, like other axes, no matter the nature of the layers boundaries, an every early flow time (infinite-acting flow time) the generally applicable source function is an infinite plane source in an infinite reservoir given as

$$s(z_{Dj}, t_{Dj}) = \frac{1}{2\sqrt{\pi t_{Dj}}} e^{-\frac{(z_{Dj}-z_{wDj})^2}{4t_{Dj}}} \tag{2.5}$$

The dimensionless parameters used are based on wellbore half-length as follows:

$$(1) \quad m_D = \frac{2m}{L} \sqrt{\frac{k}{k_m}} \quad \text{where } m = x, y, z \tag{2.6}$$

$$(2) \quad t_D = \frac{4kt}{\phi \mu c_i L^2} \tag{2.7}$$

$$(3) \quad L_D = \frac{L}{2h} \sqrt{\frac{k}{k_x}} \tag{2.8}$$

$$(4) \quad h_D = \frac{2h}{L} \sqrt{\frac{k}{k_z}} \tag{2.9}$$

$$(5) \quad p_{Dj} = \frac{p_j - p(x, y, z, t)}{\Delta p_j} \tag{2.10}$$

With these source functions the dimensionless pressure for each layer is therefore obtained for 3D flow the Newman's product method as

$$p_{Dj}(x_D, y_D, z_D, t_{Dj}) = 2\pi h_{Dj} \int_0^D s(x_{Dj}, \tau) s(y_{Dj}, \tau) s(z_{Dj}, \tau) d\tau \tag{2.11}$$

for a constant production or injection rate. To correct for differences in flow times in the two layers as a result of possible differences in flow and layers properties, a common time frame is established by the following definition

$$t_{Di+1} = \beta t_{Di} = \beta t_D \tag{2.12}$$

Therefore,

$$\beta = \frac{\phi_i c_{ii} \mu_i L_i^2 k_{i+1}}{\phi_{i+1} c_{i+1} \mu_{i+1} L_{i+1}^2 k_{i+1}} \tag{2.13}$$

### 3.0 Individual Layer Dimensionless Pressure Expressions

#### 3.1 Crossflow Interface

The layers dimensionless pressure expressions are derived according to equation (2.11) as follows:

##### 3.1.1 Layer *i* (Bottom Layer)

$$p_{Di}(x_D, y_D, z_D, t_D) = \frac{E_i \sqrt{\pi t}}{2} \int_0^D \left[ \operatorname{erf} \left( \frac{1+x_D}{2\sqrt{\tau}} \right) + \operatorname{erf} \left( \frac{1-x_D}{2\sqrt{\tau}} \right) \right] e^{-\frac{(y_D - y_{wD})^2}{4\tau}} \frac{1}{\sqrt{\tau}} \sum_{n=1}^{\infty} \exp \left( -\frac{(2n+1)^2}{4h_D^2} \pi^2 \tau \right) \cos(2n+1) \pi \frac{z_D}{h_D} \cos(2n+1) \pi \frac{z_{wD}}{h_D} d\tau \tag{3.1}$$

##### 3.1.2 Layer *i* + 1 (Upper Layer)

$$p_{Di+1}(x_D, y_D, z_D, t_D) = \frac{E_i \sqrt{\pi \beta}}{2} \int_0^D \left[ \operatorname{erf} \left( \frac{1+x_D}{2\sqrt{\beta \tau}} \right) + \operatorname{erf} \left( \frac{1-x_D}{2\sqrt{\beta \tau}} \right) \right] e^{-\frac{(y_D - y_{wD})^2}{4\tau}} \frac{1}{\sqrt{\tau}} \sum_{n=1}^{\infty} \exp \left( -\frac{(2n-1)^2}{4h_D^2} \pi^2 \beta \tau \right) \sin \frac{1}{2} (2n-1) \pi \frac{z_D}{h_D} \sin \frac{1}{2} (2n-1) \pi \frac{z_{wD}}{h_D} d\tau \tag{3.2}$$

Application of the following interface conditions include

(a) pressure equilibrium

$$p_{Di}(x_D, y_D, z_D = h_{Di}, t_D) = p_{Di+1}(x_D, y_D, z_D = h_{Di}, t_D) \tag{3.3a}$$

and

(b) equal flow velocities, from Darcy's law



$$\frac{\partial p_{Di}(x_D, y_D, z_D = h_{Di}, t_D)}{\partial z_D} = -M \frac{\partial p_{Di}(x_D, y_D, z_D = h_{Di}, t_D)}{\partial z_D} \tag{3.3b}$$

to equations (3.1) and (3.2) yields an eigen value, M, through a zero determinant as

$$M = \frac{I_1 \cdot I_{22}}{I_2 \cdot I_{11}} \tag{3.4}$$

The eigen value, which is the mobility ratio, prescribes the stability condition for fluid displacement through the layers. Solving equations (3.1) and (3.2) using initial and boundary (no-flow) conditions stated respectively as

$$p_{Dj}(x_D, y_D, z_D, t_D) = 0 \text{ and } \frac{\partial p_{Dj}(x_D, y_D, z_D = h_D \text{ and } z_D = 0, t_D)}{\partial z_D} = 0, \text{ we have that } E_j = E_{i+1}. \text{ At}$$

the wellbore, equation (2.10) gives unit dimensionless pressure drop in each layer at  $t_{iD} > 0$ . Therefore, representing equation (2.10) in form of Fourier series we have, for the wellbore

$$\sum_{n=1}^{\infty} p_{wDj}(x_D, y_{wD}, z_{wD}, t_{Dj}) = 1 \tag{3.5}$$

Using equations (3.1) and (3.2) equation (3.5) is solved to yield [8]

$$E_j = \frac{2}{\sqrt{\pi}} \left[ \frac{\int_{z_{wDi}}^{h_{Di}} I_{11} dz_D + \int_{h_{Di}}^{h_D} I_{22} dz_D}{\int_{z_{wDi}}^{h_{Di}} I_{11}^2 dz_D + \int_{h_{Di}}^{h_D} I_{22}^2 dz_D} \right] \tag{3.6}$$

The expression for E in equation (3.6) is imposed on equations (3.1) and (3.2) to duplicate the actual effects of the interface on the pressure distribution. In equation (3.6)

$$I_1 = \frac{1}{h_{Di}} \int_0^{t_D} \left[ \operatorname{erf}\left(\frac{1+x_{Di}}{2\sqrt{\tau}}\right) + \operatorname{erf}\left(\frac{1-x_{Di}}{2\sqrt{\tau}}\right) \right] e^{-\frac{(y_{Di} - y_{wDi})^2}{4\tau}} \frac{1}{\sqrt{\tau}} \sum_{n=1}^{\infty} (2n+1)\pi \exp\left(-\frac{(2n+1)^2}{4h_{Di}^2} \pi^2 \tau\right) \cos(2n+1)\pi \frac{z_{wDi}}{h_{Di}} \sin(2n+1)\pi \frac{z_{Di}}{h_{Di}} d\tau \tag{3.7}$$

$$I_2 = \frac{\sqrt{\beta}}{h_{Di+1}} \int_0^{t_D} \left[ \operatorname{erf}\left(\frac{1+x_{Di+1}}{2\sqrt{\beta\tau}}\right) + \operatorname{erf}\left(\frac{1-x_{Di+1}}{2\sqrt{\beta\tau}}\right) \right] e^{-\frac{(y_{Di+1} - y_{wDi+1})^2}{4\beta\tau}} \frac{1}{\sqrt{\tau}} \sum_{n=1}^{\infty} \frac{(2n-1)}{2} \pi \exp\left(-\frac{(2n-1)^2}{4h_{Di+1}^2} \pi^2 \beta\tau\right) \cos\left(\frac{2n-1}{2}\pi \frac{z_{Di+1}}{h_{Di+1}}\right) \sin\left(\frac{2n-1}{2}\pi \frac{z_{wDi+1}}{h_{Di+1}}\right) d\tau \tag{3.8}$$

$$I_{11} = \int_0^{t_D} \left[ \operatorname{erf}\left(\frac{1+x_{Di}}{2\sqrt{\tau}}\right) + \operatorname{erf}\left(\frac{1-x_{Di}}{2\sqrt{\tau}}\right) \right] e^{-\frac{(y_{Di} - y_{wDi})^2}{4\tau}} \frac{1}{\sqrt{\tau}} \sum_{n=1}^{\infty} \exp\left(-\frac{(2n+1)^2}{4h_{Di}^2} \pi^2 \tau\right) \cos(2n+1)\pi \frac{z_{wDi}}{h_{Di}} \cos(2n+1)\pi \frac{z_{Di}}{h_{Di}} d\tau \tag{3.9}$$

$$I_{22} = \sqrt{\beta} \int_0^{t_D} \left[ \operatorname{erf} \left( \frac{1+x_{Di+1}}{2\sqrt{\beta\tau}} \right) + \operatorname{erf} \left( \frac{1-x_{Di+1}}{2\sqrt{\tau\beta}} \right) \right] e^{-\frac{(y_{Di+1} - y_{wDi+1})^2}{4\beta\tau}} \frac{1}{\sqrt{\tau}} \sum_{n=1}^{\infty} \frac{(2n-1)}{2} \pi \exp \left( -\frac{(2n-1)^2}{4h_{Di+1}^2} \pi^2 \beta\tau \right) \sin \left( \frac{2n-1}{2} \pi \frac{z_{wDi+1}}{h_{Di+1}} \right) \sin \left( \frac{2n-1}{2} \pi \frac{z_{Di+1}}{h_{Di+1}} \right) d\tau \quad (3.10)$$

### 3.1.3 No Crossflow Interface

When there is an impermeable interface each layer behaves like an independent reservoir. The layers are commingled in a common (parent) wellbore. Therefore, the dimensionless pressure expressions for the layers are

$$P_{Dj}(x_{Dj}, y_{Dj}, z_{Dj}, t_D) = \frac{\sqrt{\pi}}{4} \int_0^{t_D} \operatorname{erf} \left( \frac{1+x_{Dj}}{2\sqrt{\tau}} \right) + \operatorname{erf} \left( \frac{1-x_{Dj}}{2\sqrt{\tau}} \right) e^{-\frac{(y_{Dj} - y_{wDj})^2}{4\tau}} \left[ 1 + \frac{1}{2} \sum_{n=1}^{\infty} \exp \left( -\frac{n^2 \pi^2 \tau}{4h_{Dj}^2} \right) \cos n\pi \frac{z_{Dj}}{h_{Dj}} \cos n\pi \frac{z_{wDj}}{h_{Dj}} \right] d\tau \quad (3.11)$$

where  $j = \text{layer } i \text{ or } i + 1$

### 4.0 Early Radial Period Pressure Approximations

When no boundary of any kind has been felt, the pressure behaviour is similar to one obtainable in an infinite reservoir. No matter how thin a reservoir may be and no matter how small and short the well radius and length are, this behaviour must be exhibited at the instance a well is opened until the nearest boundary is felt. During this period, the reservoir pressure changes rapidly with time, and

$$P_D = \frac{\alpha h_D}{8} \int_0^{t_D} e^{-\frac{(z_D - z_{wD})^2 + (z_D - z_{wD})^2}{4\tau}} \frac{1}{\sqrt{\tau}} d\tau \quad (4.1)$$

which yields the exponential integral solution

$$P_D = \frac{-\alpha h_D}{8} E_i \left( -\frac{R^2}{4t_D} \right) \quad (4.2)$$

where  $\alpha = 2$  if  $x_D < 1$ , 1 if  $x_D = 1$ , and 0 if  $x_D > 1$ .  $R^2 = (z_D - z_{wD})^2 + (z_D - z_{wD})^2$

### 5.0 Early Linear Period Pressure Approximations

#### 5.1 Crossflow

When there is crossflow between the layers, the entire reservoir will behave as one enlarged reservoir, especially when the entire interface length is permeable. Early linear period pressure distribution is achieved at

$t_D$  corresponding to  $\left( \frac{1+x_D}{2\sqrt{t_D}} \right) \geq 1.8$ . Beyond this time, flow is flourishing in the x-y plane. This, however,

occurs at top of the entire reservoir, that is, at  $h_D = h_D + h_{Di+1}$ .



5.2 **No Crossflow**

The early linear period occurs for each layer after the top of the layer is felt by flow transients. Here, at this time, the error function is less than unit.

6.0 **Computation of Well Responses**

All integrations with respect to time were performed numerically according to the suggestions in [8] and [9]. It should be noted that  $h_{Dj} \leq z_{Dj} + z_{wDj} < h_D$ , and that the dimensionless times for start or end of a particular flow period can best estimated from a plot of  $p_D$  against  $\log(t_D)$ . Pressure distribution observed shortly after these periods will reveal the actual nature of the reservoir boundaries. To simulate an infinite-conductivity wellbore [12]  $x_{Dj} = 0.732$ ;  $0 \leq x_{Dj} < 0.732$  represent uniform flux wellbore. For dimensionless wellbore pressures very small values of wellbore widths,  $y_{wD}$  and radii are used because the wells are line sources.  $x_D \geq 2$  means full well penetration along the x-direction. When interlayer flow situations are considered, for example, in both secondary and tertiary recovery projects, the actual values of  $\beta$  are calculated for a given set of reservoir and wellbore properties, using equation (2.13). The final dimensionless pressure is obtained by superposition of the dimensionless pressures due to (1) early time behaviour (from  $t_D = 0$  to  $t_D = \infty$ , and (2) any other flow period possible within the flow time of interest.

7.0 **Discussion of Results**

7.1 **Effects of Well stand-off  $z_{wD}$  on  $p_{wD}$**

Dimensionless wellbore pressure  $p_{wD}$  were generated for both crossflow and no-crossflow systems. The results are shown in Tables 1 to 2 respectively. From the results, it is clear that dimensionless wellbore pressures are unaffected by well locations.

7.2 **Effects of Wellbore Radius on  $p_{wD}$**

To understand the effects of wellbore radius on wellbore pressure,  $p_{wD}$  values were computed for  $r_{wD}$  values of  $5 \times 10^{-5}$ ,  $10^{-4}$  and  $5 \times 10^{-4}$  (in an increasing order) for crossflow layers with different thickness. The wellbore dimensionless length,  $L_D$  is the reciprocal of  $h_D$ . The well responses are shown in Tables 3 and 4. Using the same thickness well responses were also computed for no crossflow layers. The results for the no crossflow case are shown in Table 5.

From the results in Tables 3 and 5, it is clear in all cases that layer  $p_{wD}$  values are obtained with smaller wellbore radius. The differences in  $p_{wD}$  values are significant at early times and reduce to less significant values at late times. For example, in Table 5, the differences are about 20% at early times and less than 7% at late times. It is noticed, too, that the thicker the reservoir the larger the dimensionless wellbore pressures. Therefore, based on wellbore half-length, narrow wells offer excellent productivities at early times.

7.3 **Effect of Well length on Well Response**

To study the effect of length on well responses, well responses for cross flow and no-cross flow were computed for reservoir dimensionless thickness of 0.8, 1.2, 2.0 and 3. These translate to dimensionless well lengths of 1.25, 0.83, 0.5 and 0.33, respectively, for an isotropic reservoir layers. Well stand-off values were 0.2, 0.3, 0.5 and 0.75 for a fixed value of  $r_{wD} = 5 \times 10^{-5}$ . The results are shown below in Tables 6a and 6b. As discussed in [5] and [12], and revealed also in Tables 6a and 6b, the longer the wellbore lengths, the lower the productivities for fixed values of  $z_{wD}$  and  $r_{wD}$ . Long wells produce the effects of pressure transient attenuation; from the point of measurement the wellbore pressure transient decreases as the length of propagation increases. At early times the effects of well length, in both crossflow and no-crossflow systems are exactly the same as no boundary is felt. At long times, however, when different boundaries are encountered, the  $p_{wD}$  values increase in equal amounts but those of no-crossflow are larger in magnitude.



### 8.0 Detection of Layering and Crossflow

To detect crossflow, first plot  $p_{wD}$  versus  $t_D$  on semi-log paper for crossflow for each layer. If crossflow is established, then make the plot for only crossflow case for each layer. Match each curve with those from observed (well flow pressures against time) plot and calculate the permeability for each layer. Equal permeability values mean absence of layering. Different permeability values mean presence of layering. This approach is discussed and used in [17] and [14].

As shown in Tables 7 and 8, for the layered reservoir with crossflow the  $p_{wD}$  values are about the same as those of no crossflow at early times. But at late times the dimensionless wellbore pressures of no crossflow layers appreciate to between approximately 1.02 and 1.12 times those of crossflow. Furthermore, no crossflow systems exhibit earlier departure from early radial behaviour and earlier pseudosteady behaviour than crossflow system.

### 9.0 Validation of Results

Following the difference in the definition of  $z_D$  in our case and those of other authors, [12], [15], [16], a basis for comparison with these model results exist only for  $h_D = L_D = 1.0$ . For this condition, dimensionless wellbore pressures were calculated for some dimensionless wellbore parameters using our models. This basis is, however, necessary only at long times. For early times differences in dimensionless parameters definitions do not affect the results. This is because at early wellbore pressures exhibit infinite reservoir behaviour. For early times, therefore, the calculated results are compared with some other results [12], [15] and [16] as shown in Table 9. The dimensionless pressures show an acceptable closeness between all the authors (including ours).

### 10.0 Application to Displacement Stability Predictions

The unique set of operational parameters, such as wellbore properties, reservoir layers and fluid properties, which can create a delay or completely prevent breakthrough, is measured using the mobility ratio,  $M$ , derived in equation (3.4). The mobility ratio compares the velocities of both the displacing and the displaced fluids, and is usually less than unity (best condition) for any set of wellbore and fluid properties. This flow condition is referred to as favourable or stable displacement. For unfavourable or unstable displacement,  $M$  is generally greater than 10. For  $M > 10$ , the displacing fluid travels faster than oil and is produced in large volumes into the producing well. Detailed solutions of equation (3.5) for various wellbore, layers and layers' fluid properties have been discussed in [17] and [18], and are summarized below.

### 11.0 Effects of Wellbore, layers and layers fluid properties on Displacement Stability

[17] and [18] show that although, water breakthrough times are not strongly sensitive to well spacing, substantial stability can be achieved if the wells are reasonably spaced within the constraint of layers thickness. More stable front is however, achieved when both layers have equal permeability than when the top layer is more permeable. If the reservoir layers have better porosity, the dimensionless breakthrough times for these two cases are appreciable enough for a waterflood in a small and thin reservoir.

Furthermore, an arbitrary increase or decrease in well length does not necessarily lead to achieving stability or instability for the waterflood system. This unpredictable behaviour of well lengths has been found to affect even wellbore pressures in layered reservoirs, [3], [4], [5] and single-layer reservoirs [12]. With a particular set of well lengths appreciable stability could be achieved by ensuring that the well in the less permeable layer is used for injection and the other for production.

The ratios of  $\frac{c_{ji}}{c_{ji+1}}$  yield significant stability only when  $c_{ji} \gg c_{ji+1}$ . This is possible in gas

injection and thermal flooding using well  $i$  for injection. However, larger  $\frac{\mu_i}{\mu_{i+1}}$  ratios yield higher stability.

Advantage of these viscosity ratios can be taken in polymer-impregnated waterflooding using well  $i$  for injection.

### 12.0 Conclusions

Mathematical models have been formulated to describe pressure distribution in layered reservoir (with



and without crossflow) containing lateral wells. The studies reveal that

1. For crossflow layers, pressure distribution in the layers approximates that of a single layer with equivalent single layer properties.
2. The effects of wellbore properties, on overall productivity in a layered reservoir, are similar to that of a horizontal or lateral well in a single layer reservoir.
3. Crossflow layers fluid production is more economical in terms of productivity than completing individual layers for production.
4. Crossflow and layering can be detected by observation of pressure gradients and type curve matching.
5. Lateral wells in layered reservoirs can be utilized for better oil recovery,

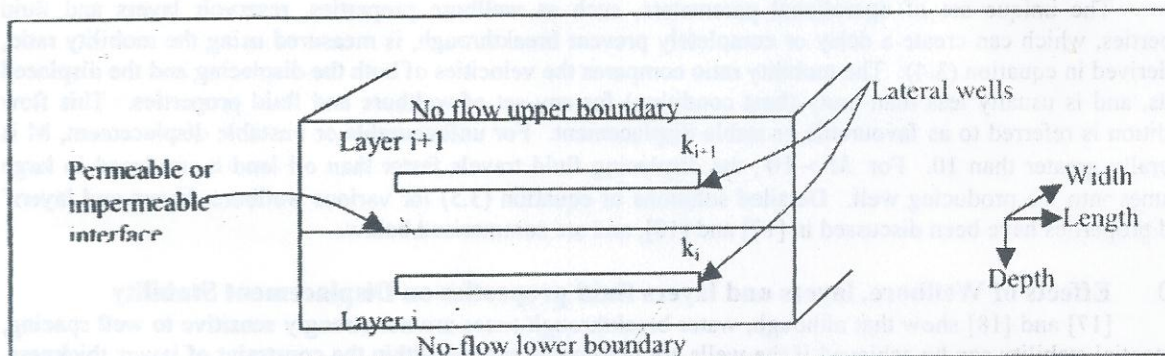
**Nomenclature**

$c$	total compressibility, $1/psi$
$E$	dimensionless weighting factor for the z-source function
$L$	wellbore length, $ft$
$k$	permeability, $md$
$h$	pay thickness, $ft$
$M$	mobility ratio
$md$	millidarcy
$p$	pressure, $psi$
$\Delta$	drop
$r$	wellbore radius, $ft$
$t$	time, $hours$
$s$	source function symbol

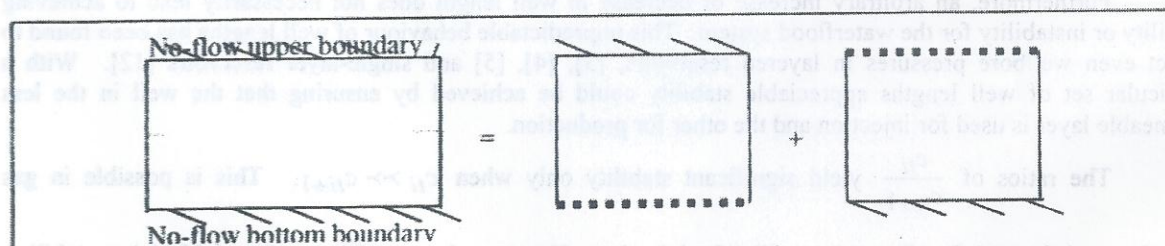
$x$	point along x-axis
$y$	point along y-axis
$z$	point along z-axis
$\phi$	porosity, $fraction$
$\mu$	viscosity, $cp$
$\tau$	dummy integration variable

**Subscripts**

$D$	dimensionless
$i$	layer $i$
$i+1$	layer $i + 1$
$j$	$i$ or $i + 1$
$t$	total
$w$	wellbore



**Fig.1: Layered Reservoir Model**



**Fig.2: Reservoir Mixed Boundaries on the z-axis.**



**Table 1: Effects of Wellbore Stand-off on  $p_{wD}$ : Cross flow layer  $i$**   
 $h_D = 2, h_{Di} = 1.0 = h_{Di+1}, y_{wDi} = y_{eDi+1} = 1 \times 10^{-4}, x_{Di} = x_{Di+1} = 1.0$

$t_D$	$z_{wDi} = 0.1$	0.2	0.6	0.8
$10^{-6}$	1.7001	1.7001	1.7001	1.7001
$10^{-5}$	2.2758	2.2758	2.2758	2.2758
$10^{-4}$	2.8514	2.8514	2.8514	2.8514
$10^{-3}$	3.4271	3.4271	3.4271	3.4271
$10^{-2}$	4.0027	4.0027	4.0027	4.0027
$10^{-1}$	4.5784	4.5784	4.5784	4.5784
1	5.1540	5.1540	5.1540	5.1540
10	5.7297	5.7297	5.7297	5.7297

**Table 2: Effects of Wellbore Stand off on  $p_{wD}$  using well  $i$  (not Crossflow)**  
 $h_{Di} = 1.0 = h_{Di+1}, y_{wDi} = y_{wDi+1} = 1 \times 10^{-4}$

$t_D$	$z_{wDi}=0.1$	0.2	0.4	0.5
0.000001	2.707	2.707	2.707	2.707
0.00001	3.858	3.858	3.858	3.858
0.0001	5.010	5.010	5.010	5.010
0.001	6.161	6.161	6.161	6.161
0.01	7.312	7.312	7.312	7.312
0.1	8.464	8.464	8.464	8.464
1	9.615	9.615	9.615	9.615
10	10.766	10.766	10.766	10.766
100	11.917	11.917	11.917	11.917

**Table 3: Effects of Wellbore radius on  $p_{wD}$  (not Crossflow)**  
 $h_D = 2, z_{wDi} = 0.7, z_{wDi+1} = 0.05, h_{Di} = 1.0, h_{Di-1} = 1.0, \beta = 1.0, x_{Di} = 0.732$

$t_D$	$r_{wDi} - r_{wDi+1} = 5 \times 10^{-5}$		$10^{-4}$		$5 \times 10^{-4}$	
	Well i	Well i+1	Well i	Well i+1	Well i	Well i+1
$10^{-6}$	1.7001	1.7001	1.3536	1.3536	0.5486	0.5486
$10^{-5}$	2.2758	2.2758	1.9292	1.9292	1.1245	1.1245
$10^{-4}$	2.8514	2.8514	2.5049	2.5049	1.7001	1.7001
$10^{-3}$	3.4217	3.4217	3.0805	3.0805	2.2758	2.2758
$10^{-2}$	4.0027	3.8643	3.6562	3.6562	2.8514	2.8514
$10^{-1}$	4.5784	4.0027	4.2318	3.5177	3.4271	3.3218
1	5.1540	4.4741	4.8075	4.1276	4.0027	4.0045



**Table 4:** Effects of Wellbore radius on  $p_{wD}$  (Crossflow) assuming one well bore  
 $h_D = 2, x_{Di} = 0.732, \beta = 1.0, z_{wDi} = 0.05,$

$t_D$	$r_{wD} = 5 \times 10^{-5}$	$10^{-4}$	$5 \times 10^{-4}$
$10^{-6}$	3.4003	2.7071	1.0977
$10^{-5}$	4.5516	3.8584	2.2490
$10^{-4}$	5.7029	5.0097	3.4002
$10^{-3}$	6.8542	6.1610	4.5516
$10^{-2}$	8.0055	7.3123	5.7029
$10^{-1}$	9.1568	8.4636	6.8542
1	10.308	9.6149	8.0055
10	11.4593	10.7662	9.1568

**Table 5:** Effects of Wellbore radius on  $p_{wD}$  (No Crossflow)  
 $h_D = L_D = 1.0, x_{Di} = 0.732, \beta = 1.0,$

$t_D$	$r_{wD} = 5 \times 10^{-5}$	$10^{-4}$	$5 \times 10^{-4}$
$10^{-6}$	17001	1.3536	0.5489
$10^{-5}$	2.2758	1.9292	1.1243
$10^{-4}$	2.8514	2.5049	1.7001
$10^{-3}$	3.4271	3.0805	2.2758
$10^{-2}$	4.1060	3.7594	2.9547
$10^{-1}$	5.5365	5.1900	4.3853
1	6.4712	6.1246	5.3199

**Table 6a:** Effects of Well length on  $p_{wD}$  (Crossflow)  $x_D = 0.732$

$L_D$	$t_D = 10^{-6}$	$10^{-5}$	$10^2$	$10^3$
1.25	1.3601	1.8206	5.0443	5.5048
0.83	2.0402	2.7310	7.5664	8.2572
0.50	3.4003	4.5516	12.6106	13.7619
0.33	5.1004	6.8274	18.9160	20.6429

**Table 6b:** Effects of Well length on  $p_{wD}$  (No Crossflow)  $x_D = 0.732$

$L_D$	$t_D = 10^{-6}$	$10^{-5}$	$10^2$	$10^3$
1.25	1.3602	1.8206	6.8514	7.3350
0.83	2.0402	2.7310	9.3735	10.0874
0.50	3.4003	4.5516	14.4177	15.5921
0.33	5.1004	6.8274	20.7231	22.4731



**Table 7: Dimensionless Wellbore Pressure (Infinite Conductivity) Crossflow (Layer *i*)**

$h_{Di+1} = h_D - h_{Di}, y_{wDi} = y_{wDi+1} = 5 \times 10^{-5}$				
$h_D =$	0.8	1.2	2.0	3.0
$h_{Di} =$	0.4	0.6	1.0	1.5
$z_{wDi} =$	0.2	0.3	0.5	0.75
$z_{Di+1} =$	0.2	0.3	0.5	0.75
$z_{Di} =$	0.2	0.3	0.5	0.75
$z_{wDi+1} =$	0.2	0.3	0.5	0.75
Dimensionless				
Time, $t_D$				
0.000001	1.3601	2.0402	3.4003	5.1004
0.00001	1.8206	2.7310	4.5516	6.8274
0.0001	2.2812	3.4217	5.7029	8.5543
0.001	2.7417	4.1125	6.8542	10.2813
0.01	3.2022	4.8033	8.0055	12.0082
0.1	3.6627	5.4941	9.1568	13.7351
1	4.1232	6.1848	10.3081	15.4621
10	4.5837	6.8756	11.4593	17.1890

**Table 8: Dimensionless Wellbore Pressure (Infinite Conductivity) No Crossflow (Layer *i*)**

$h_{Di+1} = h_D - h_{Di}, y_{wDi} = y_{wDi+1} = 5 \times 10^{-5}$				
$h_D =$	0.8	1.2	2.0	3.0
$h_{Di} =$	0.4	0.6	1.0	1.5
$z_{wDi} =$	0.2	0.3	0.5	0.75
$z_{Di+1} =$	0.2	0.3	0.5	0.75
$z_{Di} =$	0.2	0.3	0.5	0.75
$z_{wDi+1} =$	0.2	0.3	0.5	0.75
Dimensionless				
Time, $t_D$				
0.000001	1.3602	2.0402	3.4003	5.1004
0.00001	1.8206	2.7310	4.5516	6.8274
0.0001	2.2812	3.4217	5.7029	8.5543
0.001	2.7417	4.1125	6.8542	10.2813
0.01	3.2746	4.8606	8.0407	12.0782
0.1	4.1987	6.0143	9.5458	14.499
1	5.0798	7.1601	11.2569	16.7754
10	6.1954	8.4873	13.0710	18.897

**Table 9: Comparison of results of some authors for Dimensionless Wellbore Pressure**

$x_D = 0.732, y_D = 0.0005, h_D = 1.0$  (No Crossflow)

$t_D$	Ref.14.	Ref.10.	Ref.15.	Our results
0.000001	0.05490	0.05472	0.05507	0.05489
0.00001	0.1124	0.1126	0.11245	0.11245
0.0001	0.17007	0.1700	0.11260	0.17001
0.001	0.22888	0.2288	0.17098	0.22758
0.01	0.34958	0.3495	0.29164	0.29547
0.1	0.66767	0.6675	0.60972	0.66853
1	1.37630	1.3760	1.31828	1.34005



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